IN THE CLAIMS

Please amend the claims as follows:

Claims 1-12 (Cancelled).

Claim 13 (Currently Amended): A process for manufacturing an acrylic fiber comprising the steps of:

discharging a spinning feed solution comprising an acrylonitrile polymer comprising 80 wt % or more and less than 95 wt % of acrylonitrile unit in an organic solvent, into the first coagulation bath consisting of an aqueous organic solvent solution at 30 to ~~50.degree. C.~~ 50°C containing 20 to 70 wt % of an organic solvent which may be the same as or different from the organic solvent for the spinning feed solution, to form a coagulated filament;

drawing the filament from the first coagulation bath at a rate of 0.3 to 2.0 times of the discharge linear velocity of the spinning feed solution;

stretching the filament by 1.1 to 2.0 times in the second coagulation bath consisting of an aqueous organic solvent solution at 30 to ~~50.degree. C.~~ 50°C containing 20 to 70 wt % of an organic solvent which may be the same as or different from any of the two organic solvents; and

subsequently conducting wet heat stretching of the filament by three times or more.

Claim 14 (Original): The manufacturing process as claimed in Claim 13 where the concentration of the organic solvent in the first coagulation bath is 40 to 70 wt %; the drawing rate of a coagulated filament from the first coagulation bath is 0.3 to 0.6 times of the discharge linear velocity of the spinning feed solution; and the concentration of the organic solvent in the second coagulation bath is 40 to 70 wt %.

Claim 15 (Original): The manufacturing process as claimed in Claim 13 where the concentration of the organic solvent in the first coagulation bath is 20 to 60 wt %; the drawing rate of a coagulated filament from the first coagulation bath is 0.6 to 2.0 times of the discharge linear velocity of the spinning feed solution; and the concentration of the organic solvent in the second coagulation bath is 20 to 60 wt %.

Claim 16 (Original): The manufacturing process as claimed in Claim 13 where the organic solvents in the spinning feed solution, the first coagulation bath and the second coagulation bath are dimethylacetamide and the first and the second coagulation bathes are essentially at the same temperature and have essentially the same composition.

Claim 17 (Currently Amended): The manufacturing process as claimed in Claim 14 where the first and the second coagulation bathes are at the same temperature and have the same composition, and that a coordinate (X;Y) is within the area delimited by the lines represented by the following equations (1) to (3):

$$Y = -X + 105 \qquad \text{(Eq.1)}$$

$$Y = -(1/2)X + 77.5 \qquad \text{(Eq.2)}$$

$$Y = -4X + 315 \qquad \text{(Eq.3)}$$

wherein Y is the coagulation-bath temperature ~~(.degree. C.)~~ °C and X is the concentration of the organic solvent (wt %).

Claim 18 (Original): The manufacturing process as claimed in Claim 15 where a spinneret used comprises an orifice hole having a ratio A/B of 2.0 to 10.0, wherein "A" and "B" are the length of each radially branched opening arm from its center to its tip and the width of the branched opening arm, respectively.

Claim 19 (Original): The manufacturing process as claimed in Claim 15 where a spinneret used comprises an orifice hole with an flatness of 5.0 to 15.0.

Claim 20 (Original): The manufacturing process as claimed in Claim 13 where a fiber after stretching and before drying has a degree of swelling of 70 wt % or less.

Claim 21 (New): The manufacturing process as claimed in Claim 13, wherein the filament from the first coagulation bath is drawn at a rate of 0.3 to 0.6 times of the discharge linear velocity of the spinning feed solution.

Claim 22 (New): The manufacturing process as claimed in Claim 13, wherein the filament from the second coagulation bath is stretched at a rate of 1.1 to 1.5 times of the discharge linear velocity of the spinning feed solution.

Claim 23 (New): The manufacturing process as claimed in Claim 13, wherein the filament from the first coagulation bath is drawn at a rate of 0.3 to 0.6 times of the discharge linear velocity of the spinning feed solution and the filament in the second coagulation bath is stretched by 1.1 to 1.5 times.